



EUROMED 2024



Desalination for Clean Water and Energy

6–9 May 2024

Four Seasons Hotel, Sharm El Sheikh, Egypt

106

Semi-batch reverse osmosis for home-scale desalination

Jonathan Bessette, S. Shah, M. Ahmedhussain, G. Pertuz, M. Ayoub, & A. Winter

Dept. of Mechanical Engineering, Massachusetts Institute of Technology

Agenda

- **Introduction**
- **Theory**
- **Methodology**
- **Results**

India's home purifier market.

Semi-batch operation.

Design of experiments.

Operation parameters exploration.



Introduction



Families use
Point-of-Use RO
systems to
purify water.

Introduction

Drinking
Water
25% ←

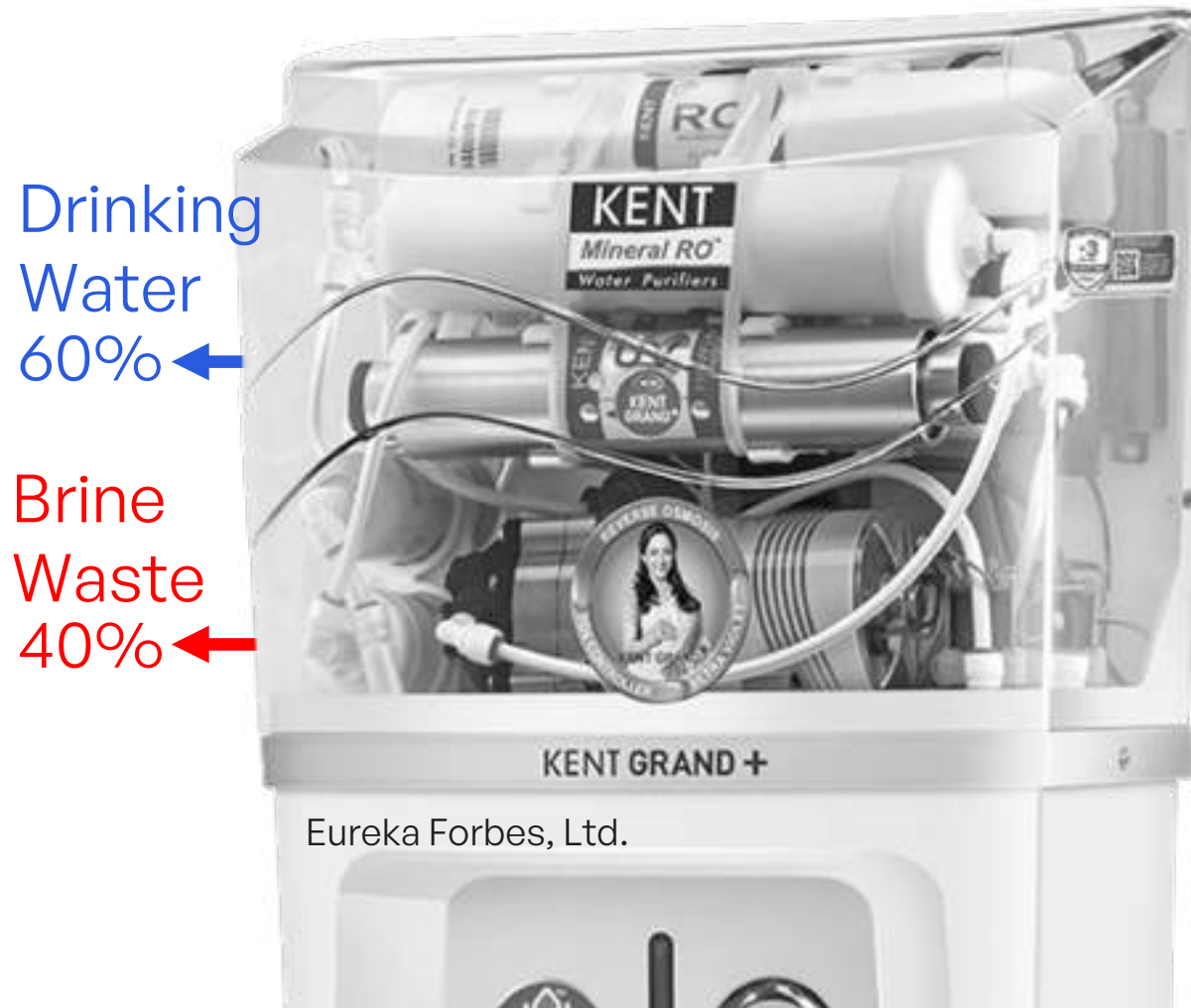
Brine
Waste
75% ←



But face the
issue of low
water efficiency
(recovery).

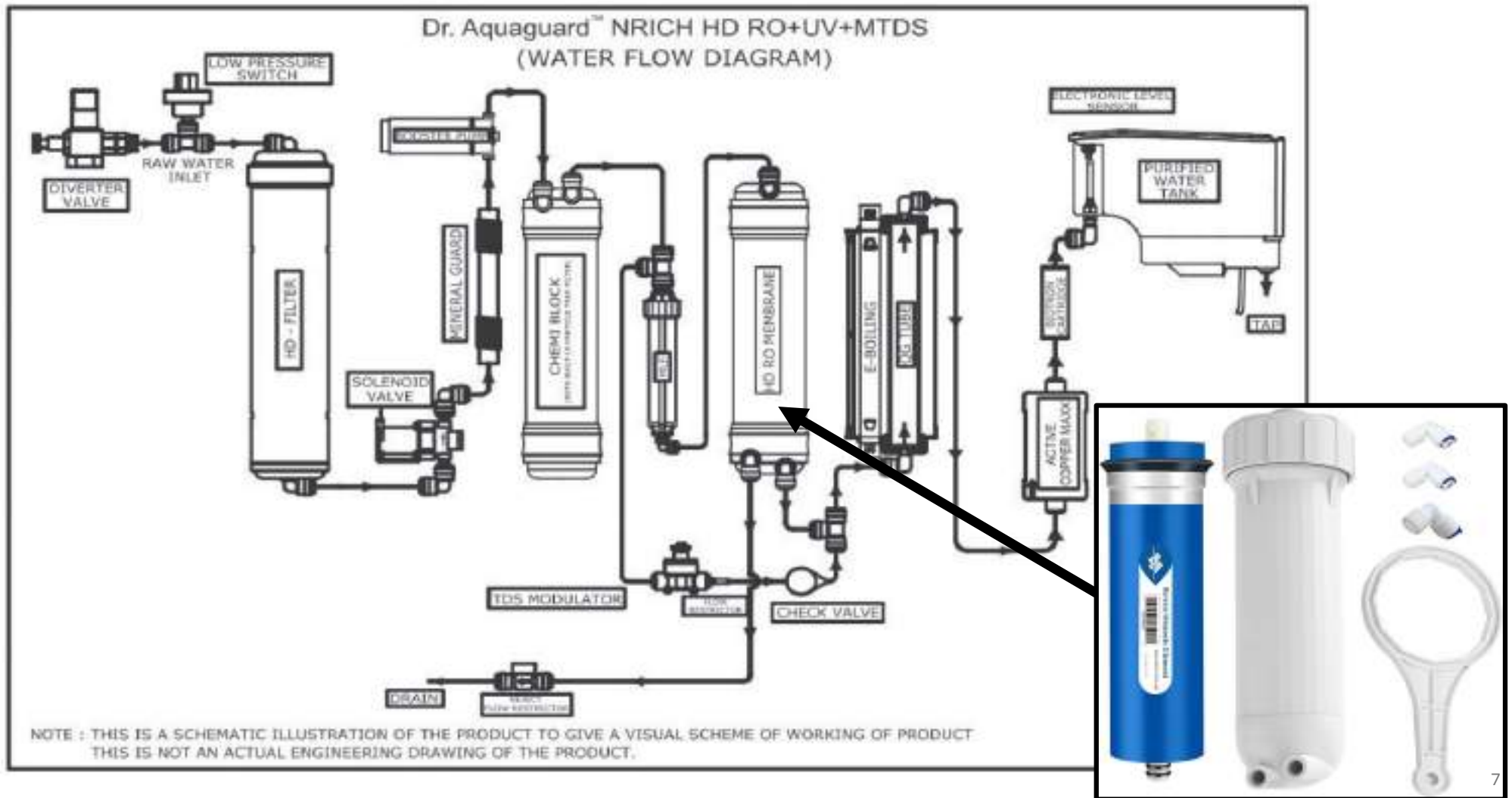
Eureka Forbes, Ltd.

Introduction



National Green Tribunal aims to mandate a **minimum of 60% recovery**, increasing to 75%+

Introduction



Theory

$$\underset{\text{Productivity}}{Q_p} = A_m * \underset{\text{Scaling}}{S} (\overset{\text{Max Pressure}}{P_f} - \pi)$$

A_m range

2-6 LMH/bar

Q_p target

12-15 LPH

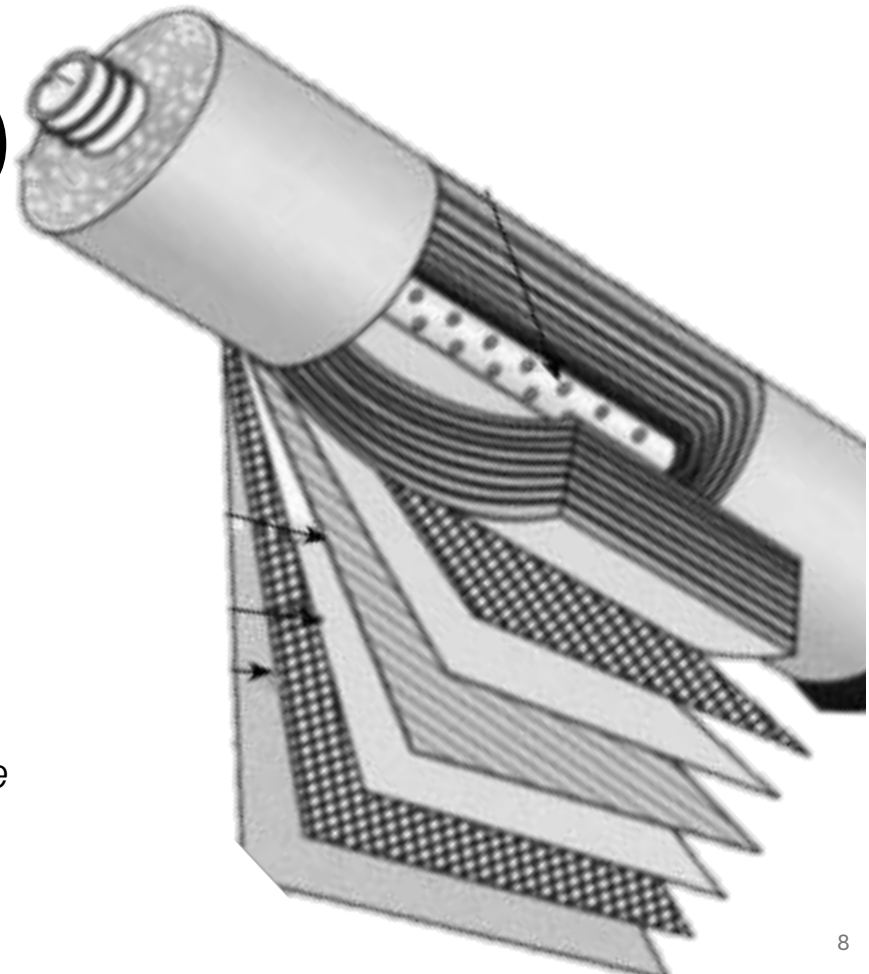
S

0.51 m² for Nano 75

π

20 psi, 1.38 bar

100 ppm ~ 1 PSI osm. pressure



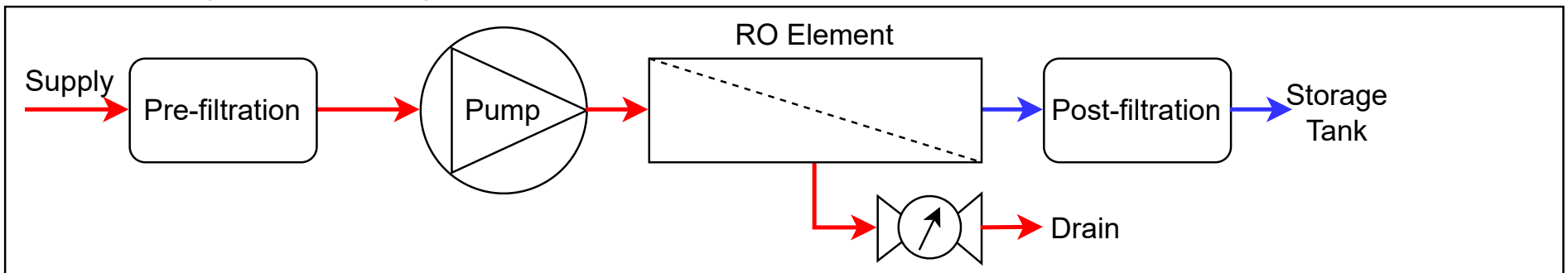
Introduction

RO recovery ratio is limited by:

- 1) RO element specifications (pressure, flux)
- 2) Scale formation, exacerbated by intermittent operation in home-scale applications

$Q_p < \text{Max. product flow rate}$
associated with maximum
membrane pressure.

Continuous (Conventional)



$Q_b > \text{Min. required brine flow}$
rate to avoid scaling

Introduction

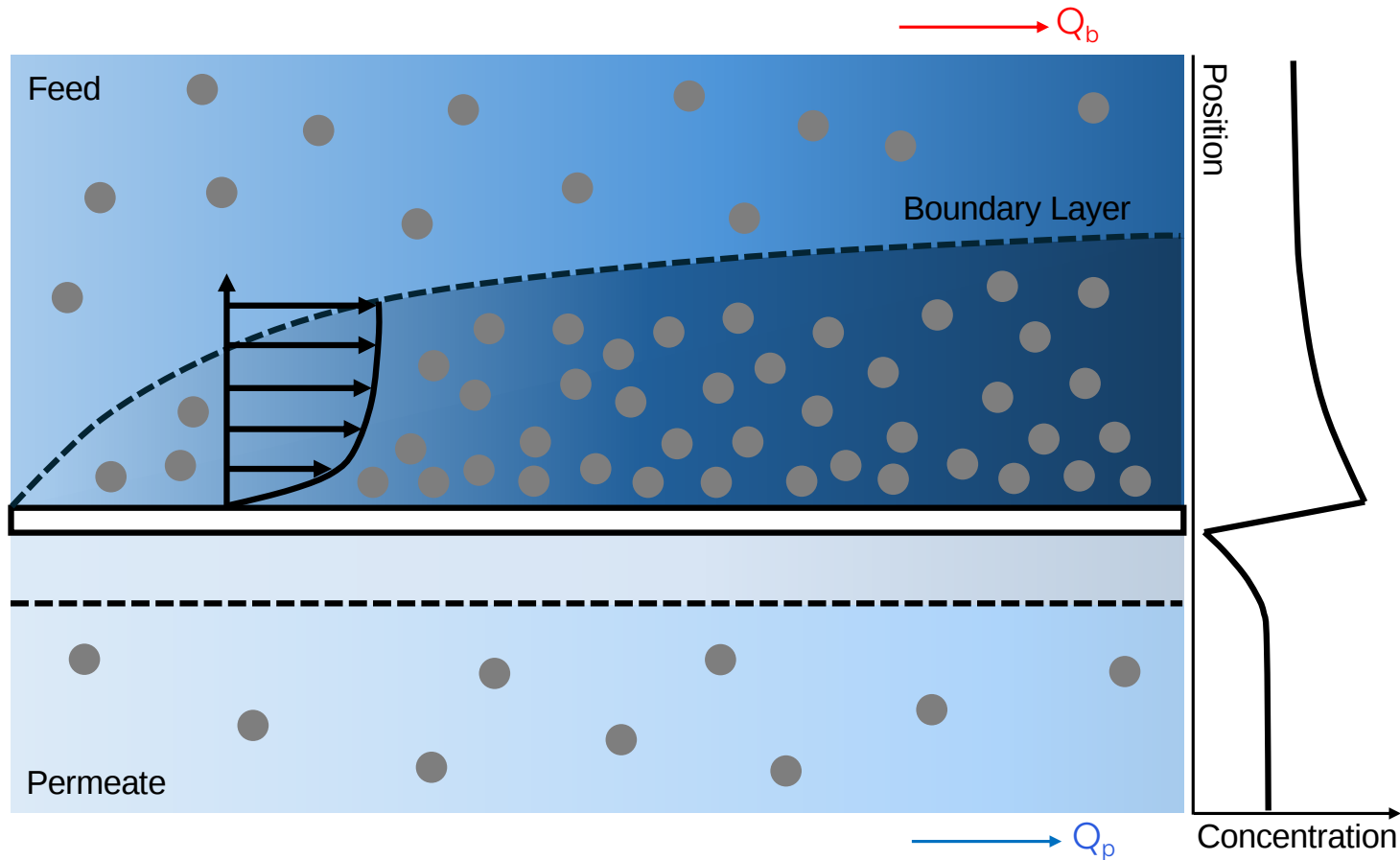
Alternative designs increase membrane area ($\uparrow S$) within an element (thus flux, $\uparrow Q_p$)

while keeping the throttle valve (brine, Q_b) the same,

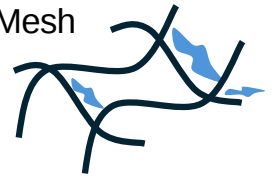
resulting in higher recovery ratio.



Introduction



Spacer Mesh



What contributes to scale formation?

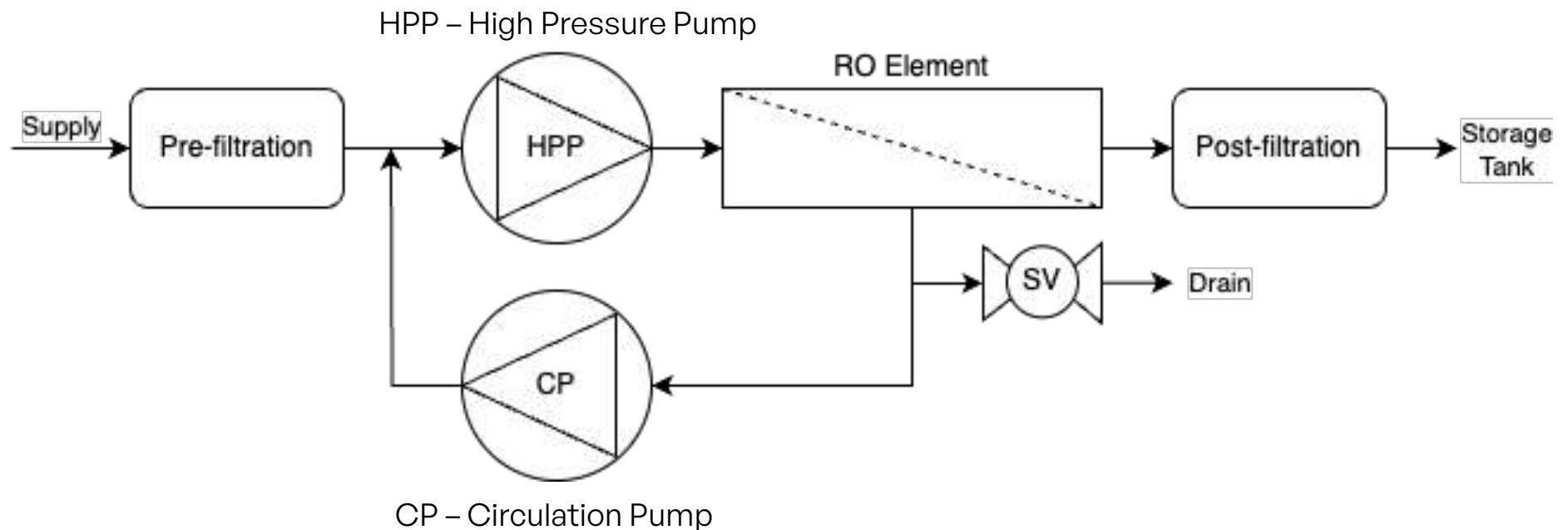
Induction time

- Flow rate
- Temperature
- Surface properties

Solution composition and concentration

Theory

Semi-batch (CCRO) Operation recirculates brine to increase recovery



Warsinger et al., 2016, “Energy Efficiency of Batch and Semi-Batch (CCRO) Reverse Osmosis Desalination,” Water Res.

Werber et al., 2017, “Can batch or semi-batch processes save energy in reverse-osmosis desalination?” Desalination, 402.

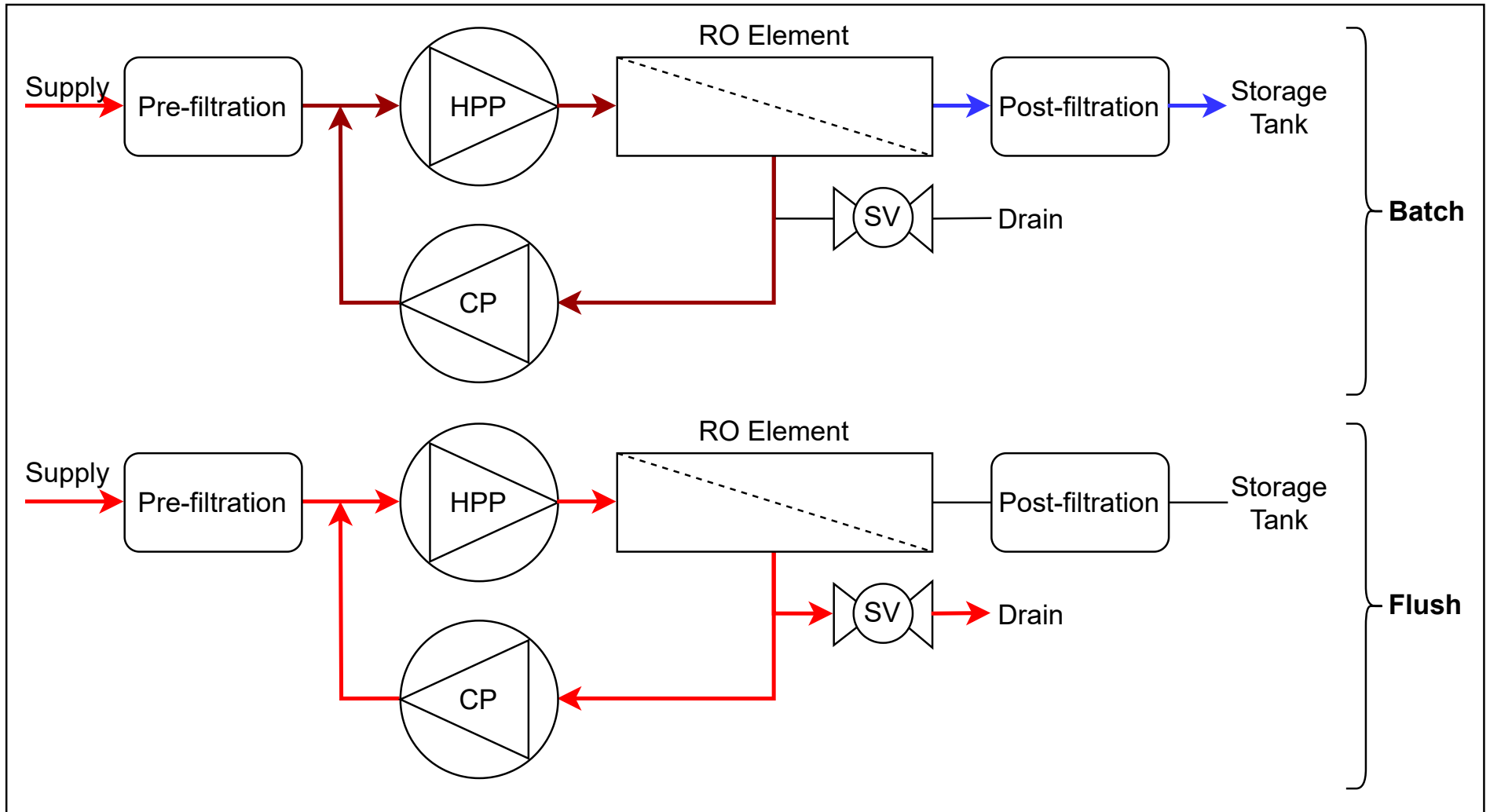
Swaminathan et al., 2019, “Practical aspects of batch RO design for energy-efficient seawater desalination.” Desalination, 470.

Wei et al., 2020, “Impact of Salt Retention on True Batch Reverse Osmosis Energy Consumption: Experiments and Model Validation,” Desalination, 479.

Lee et al., 2019, “Multi-Cycle Operation of Semi-Batch Reverse Osmosis (SBRO) Desalination,” J. Memb. Sci.

Theory

Semi-batch



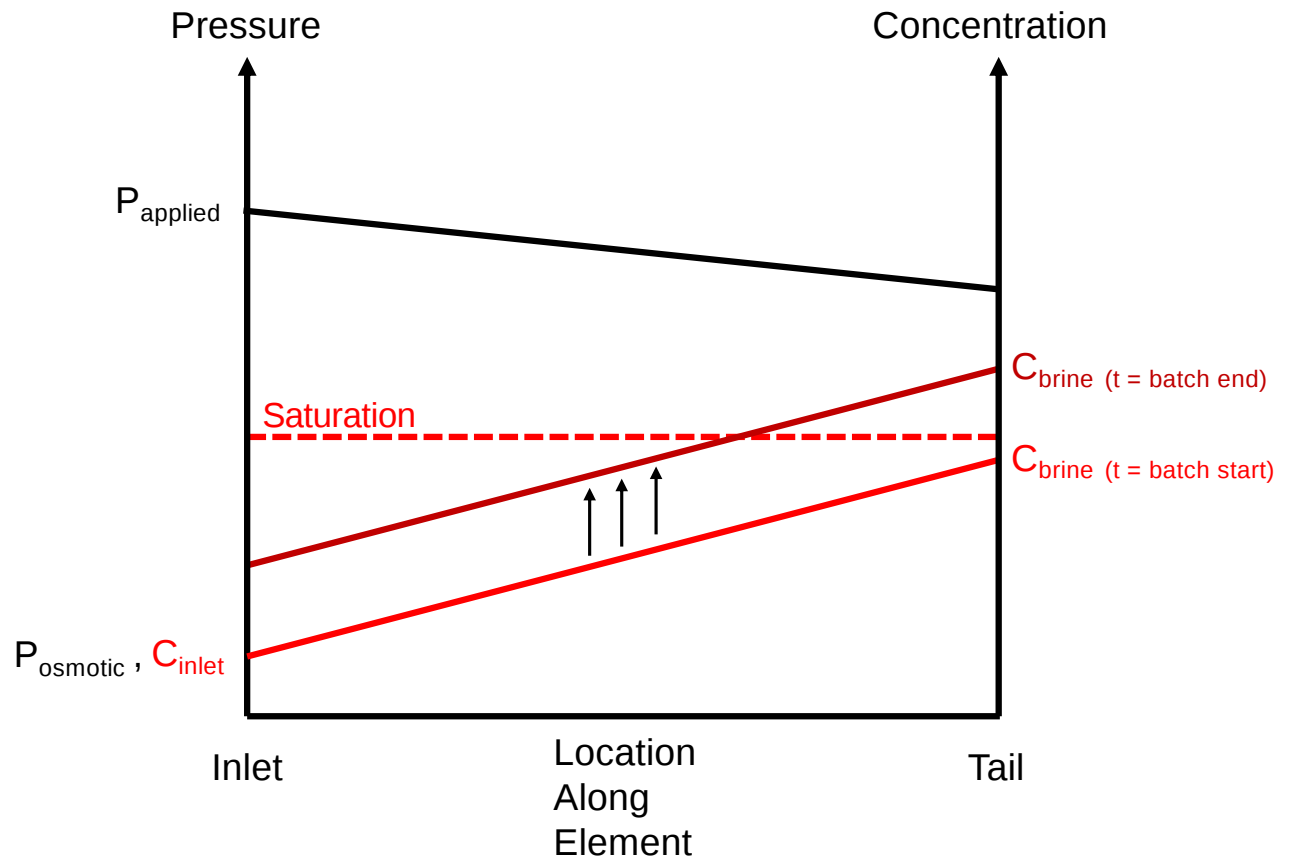
Where does scaling occur in semi-batch?

Feed pressure drops over the element

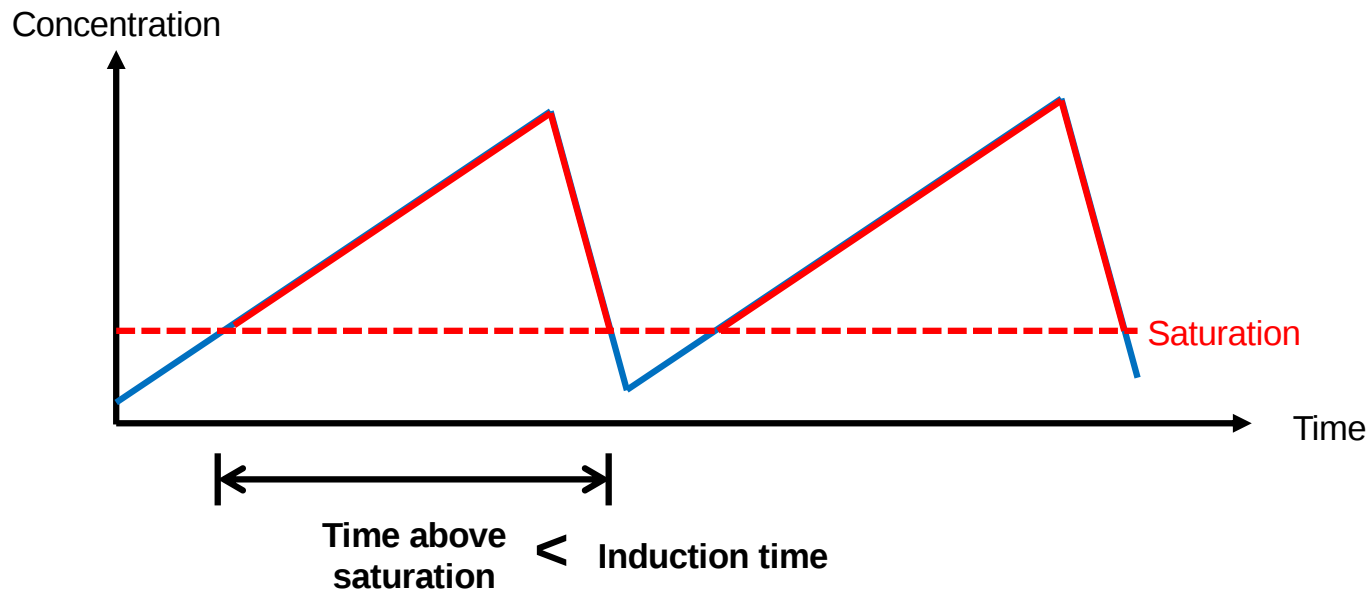
Increase in concentration (and thus, osmotic pressure) spatially, and temporally as a batch continues

Flux decreases towards the tail of the element and towards the end of the batch

Theory



Theory



Even above saturation, if we **operate under induction time** and clear salts during flush, we can prevent scaling.

Theory

Semi-batch RO

Value proposition

- Regulatory compliance (w/ recovery specification)
- Small modification to existing products, low-CAPEX change (SV, CP)
- Minimal retraining of providers
- Consistent user-experience & tech
- No increase in maintenance cost

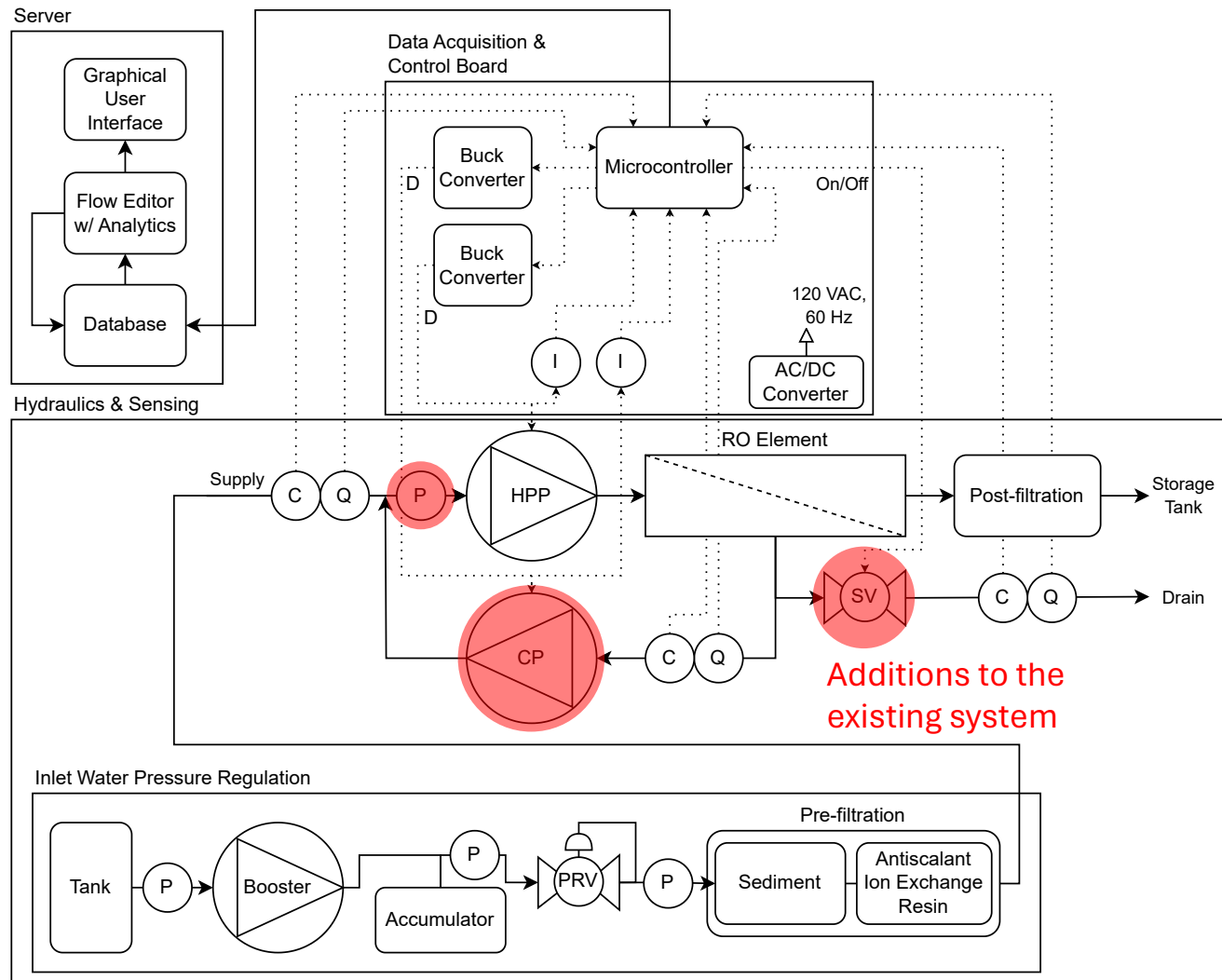
Research Questions

Semi-batch RO

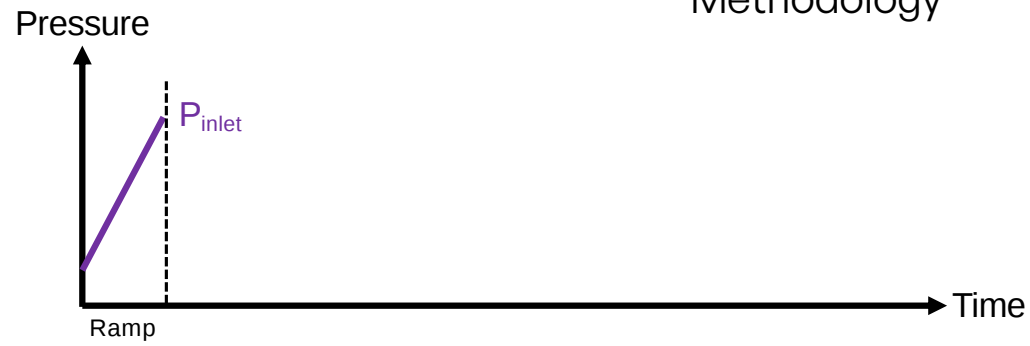
Challenges

- High-recovery semi-batch architecture
- What are the ideal control parameters & how do changing these affect performance?
 - Does the system withstand **scaling** over time and meet the current system lifetime specs?

Methodology



Methodology



$$Q_p = A_m * S (P_f - \pi)$$

Color Key

Constraints

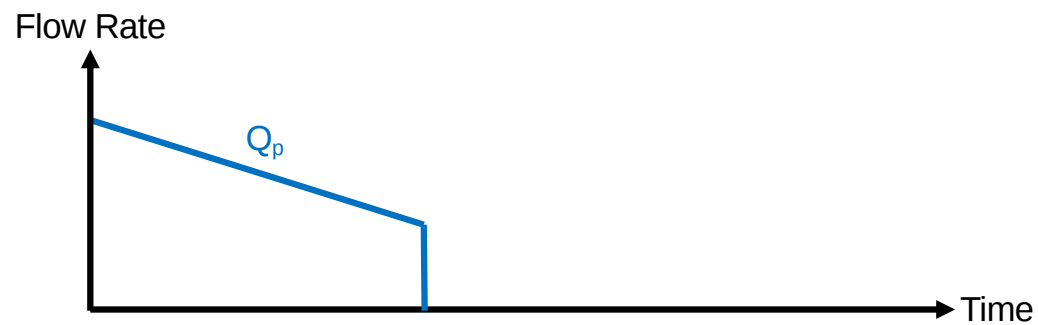
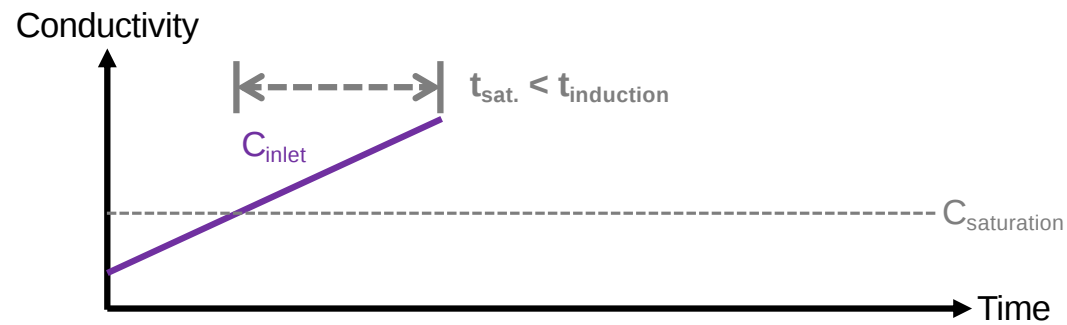
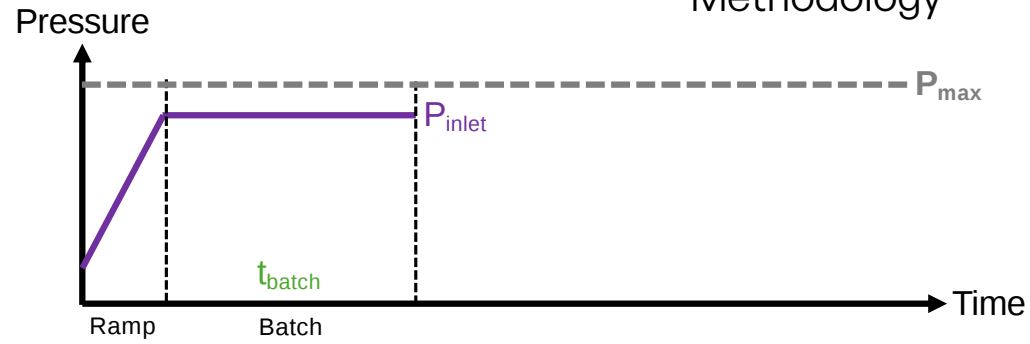
Operating parameters

Feed

Permeate

Brine

Methodology



$$Q_p = A_m * S (P_f - \pi)$$

Color Key

Constraints

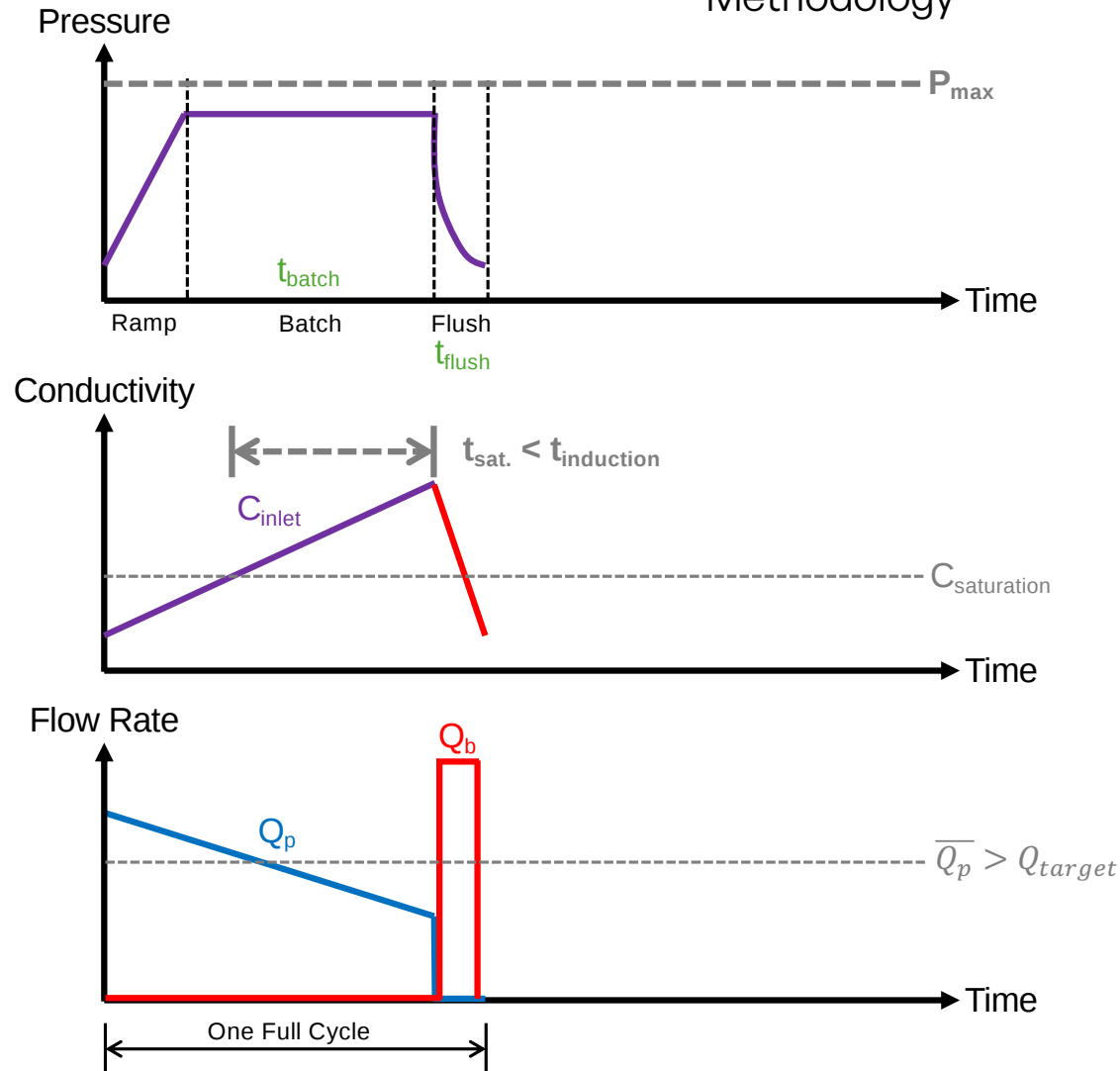
Operating parameters

Feed

Permeate

Brine

Methodology



$$Q_p = A_m * S (P_f - \pi)$$

Color Key

Constraints

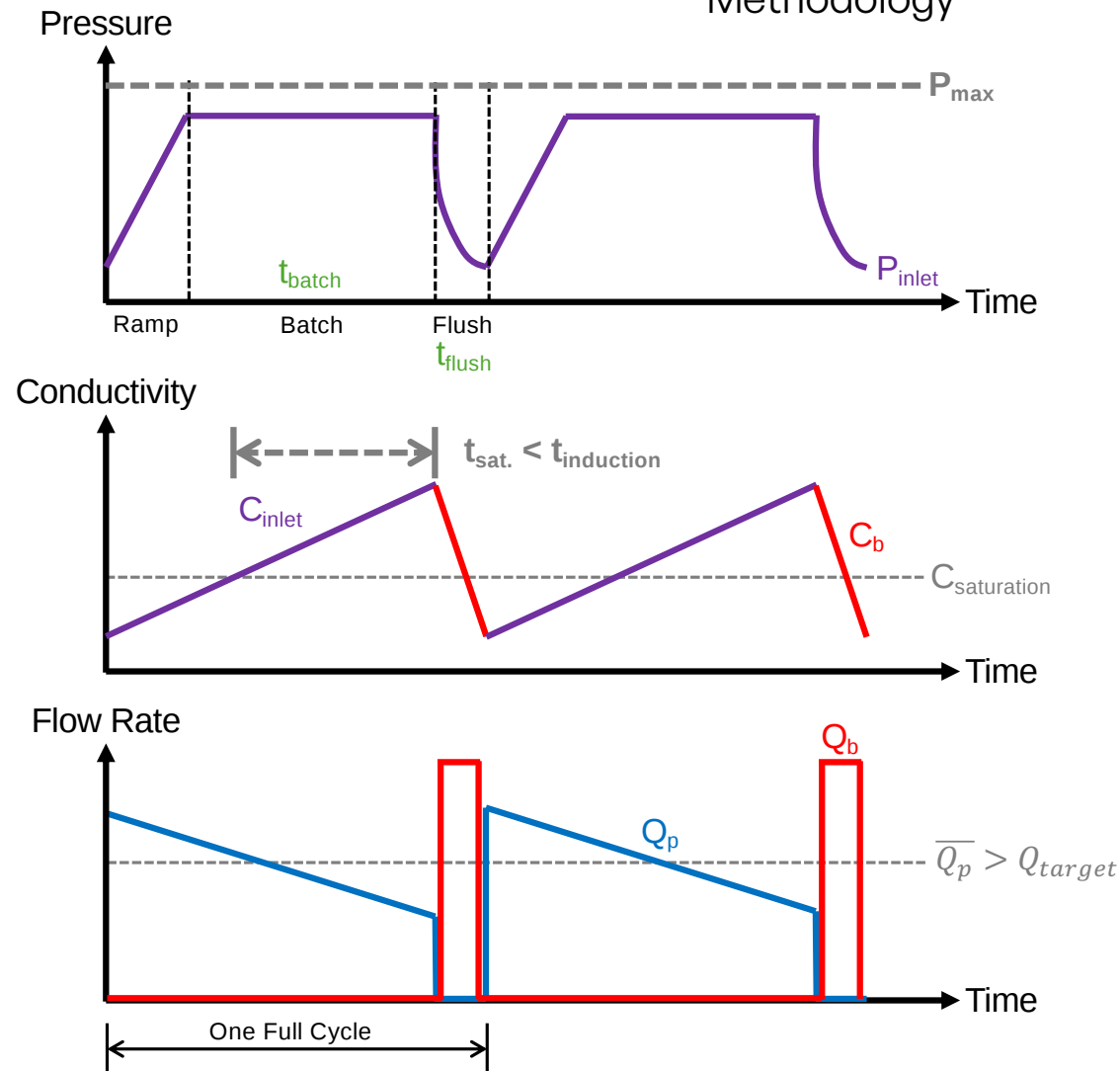
Operating parameters

Feed

Permeate

Brine

Methodology



$$Q_p = A_m * S (P_f - \pi)$$

Color Key

Constraints

Operating parameters

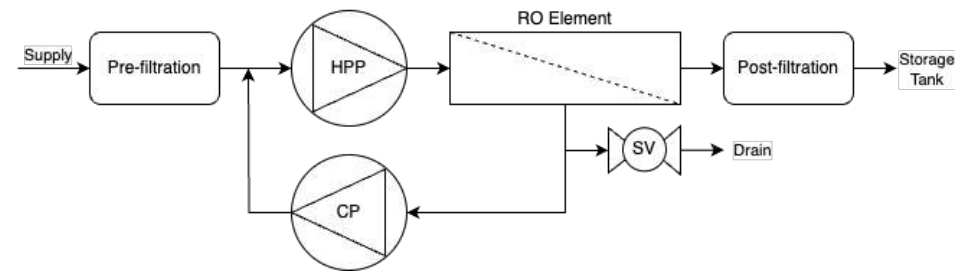
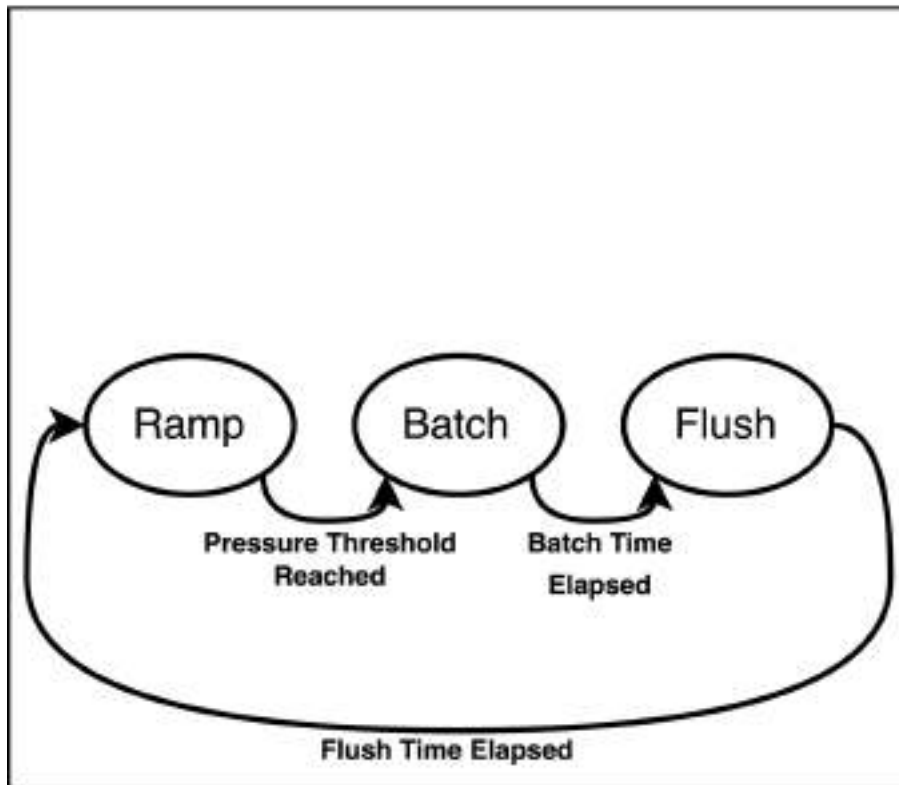
Feed

Permeate

Brine

Methodology

State Machine

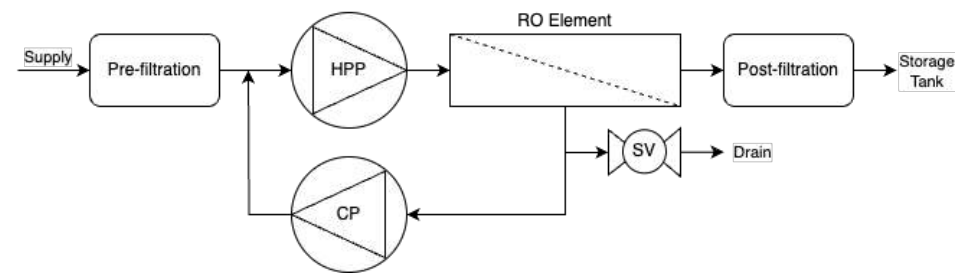
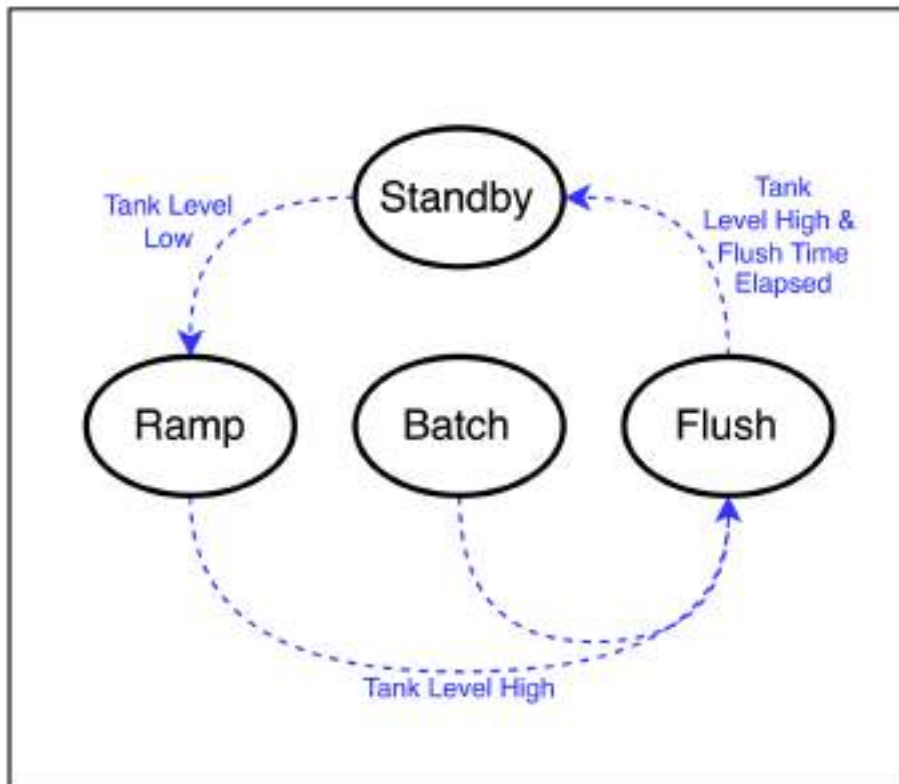


State Descriptions

Actuators	Ramp	Batch	Flush	Standby
HPP	On	Regulated	On	Off
CP	On	On	On	Off
SV	Closed	Closed	Open	Closed

Methodology

State Machine

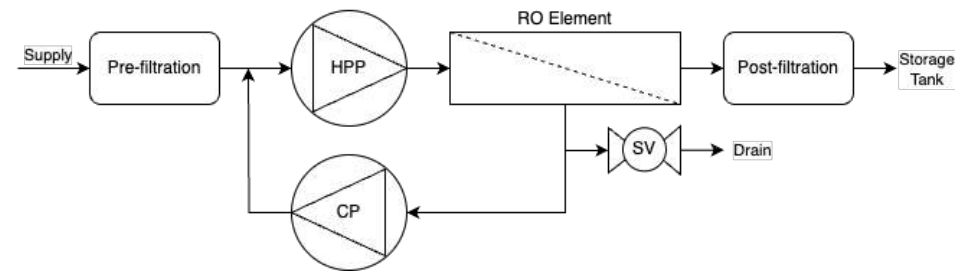
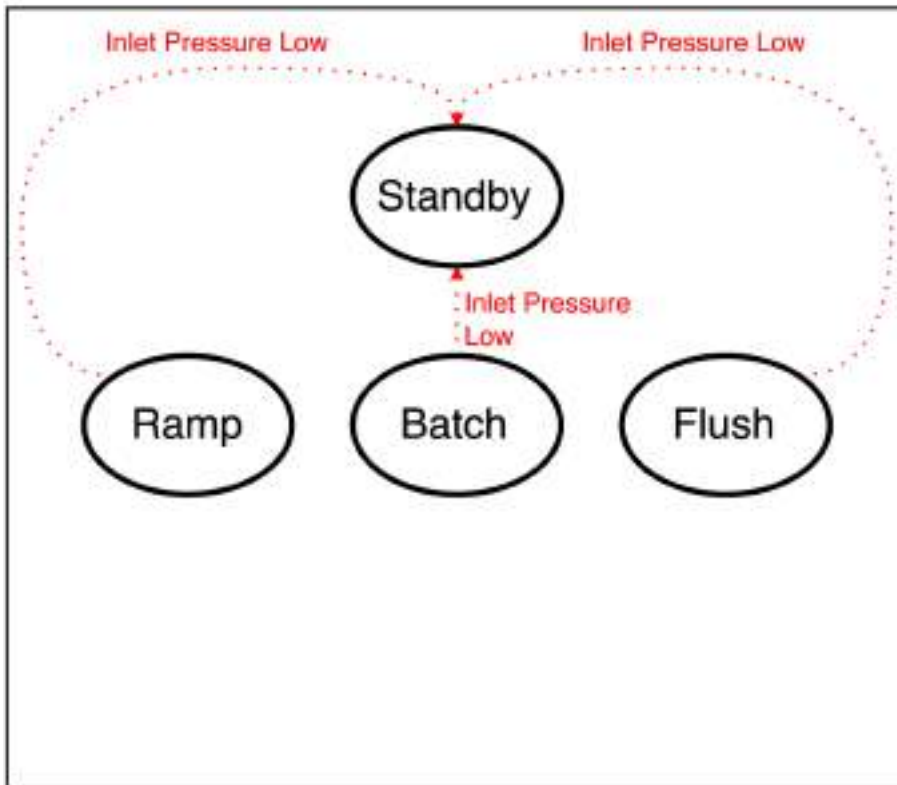


State Descriptions

Actuators	Ramp	Batch	Flush	Standby
HPP	On	Regulated	On	Off
CP	On	On	On	Off
SV	Closed	Closed	Open	Closed

Methodology

State Machine

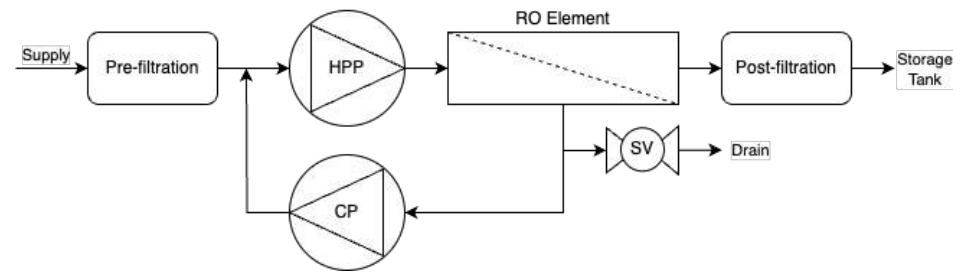
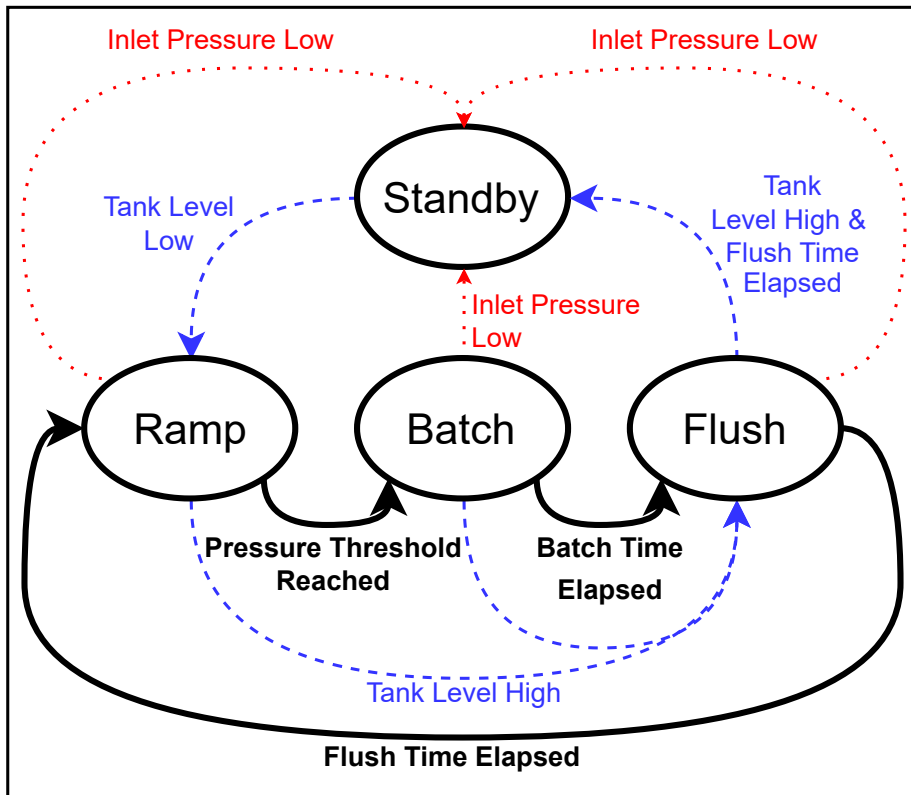


State Descriptions

Actuators	Ramp	Batch	Flush	Standby
HPP	On	Regulated	On	Off
CP	On	On	On	Off
SV	Closed	Closed	Open	Closed

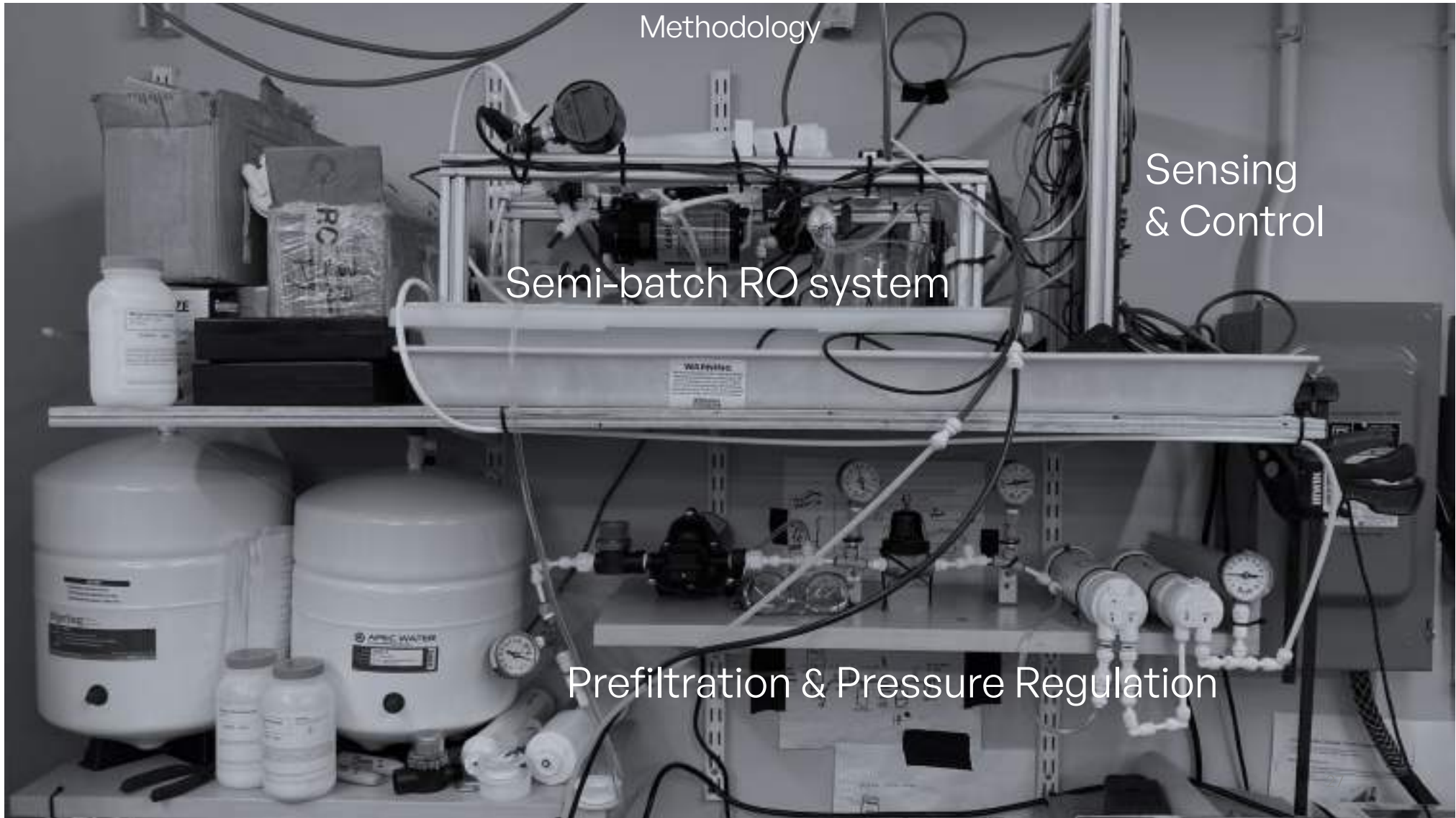
Methodology

State Machine



State Descriptions

Actuators	Ramp	Batch	Flush	Standby
HPP	On	Regulated	On	Off
CP	On	On	On	Off
SV	Closed	Closed	Open	Closed

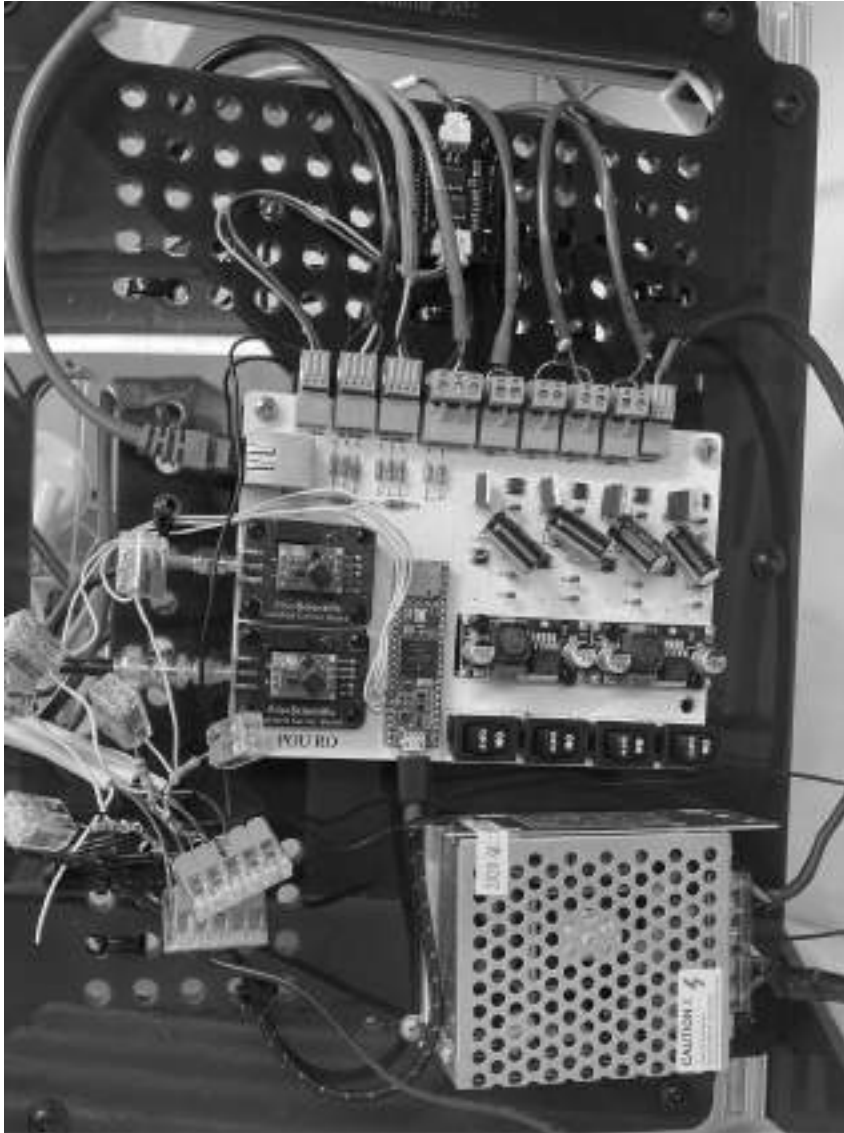


Methodology

Sensing
& Control

Semi-batch RO system

Prefiltration & Pressure Regulation



Methodology

Teensy 4.1

Import Packages

MQTT/Ethernet Init.

Read Sensors

State Machine Control

PID on Pressure within Batch State

Export Sensor Data

Methodology



Server
InfluxDB & Node-Red

Parametric Exploration (DOE)

IV

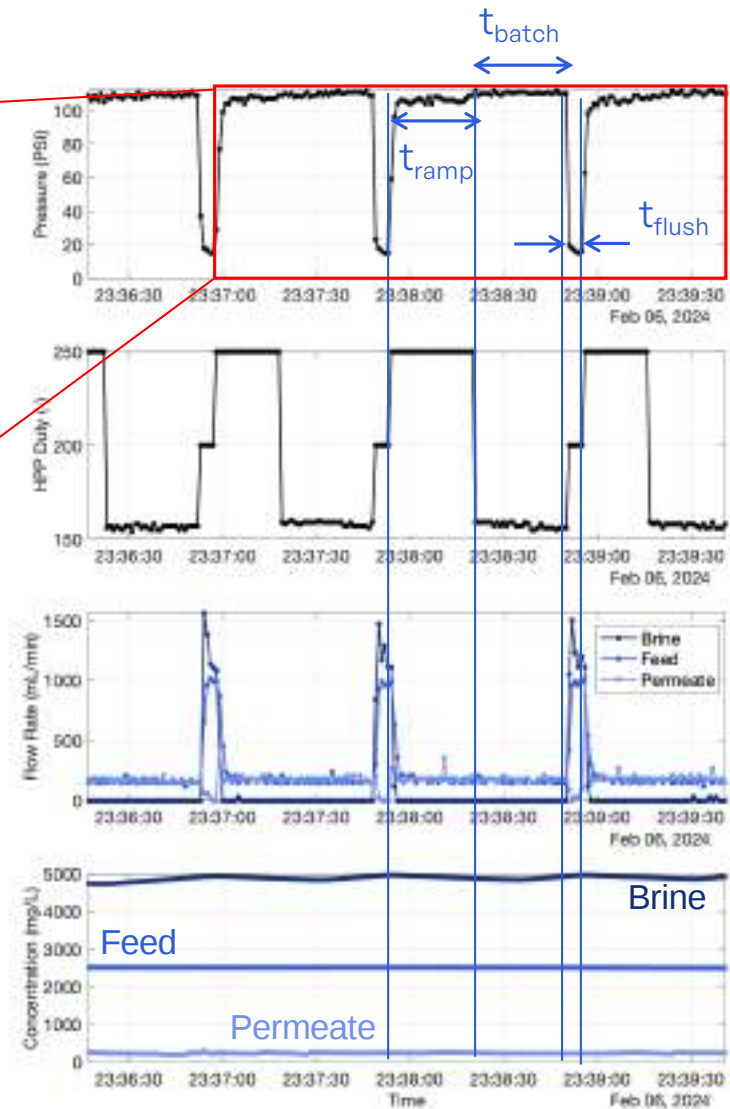
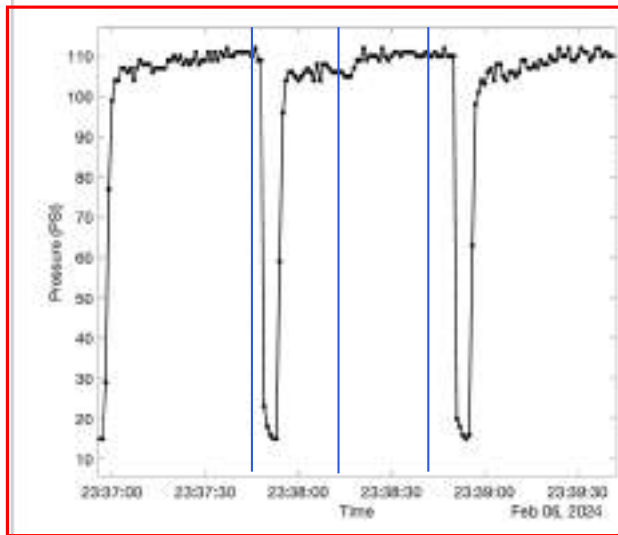
- HPP, CPP max duty
- Operating pressure & hysteresis
- Flushing time
- Batch time

DV

- Diluate, Brine volume → Recovery, Production rate
- Diluate, Brine conductivity → Scaling propensity

	Recovery	Production Rate	Scaling Propensity	Virtual Cond. & Mem. Sensing
Flush Time ↑	↓	↑	↓	↓
Batch Time ↓	↓	↑	↓	↓
Flush Time ↓	↑	↓	↑	↑
Batch Time ↑	↑	↓	↑	↑

Results



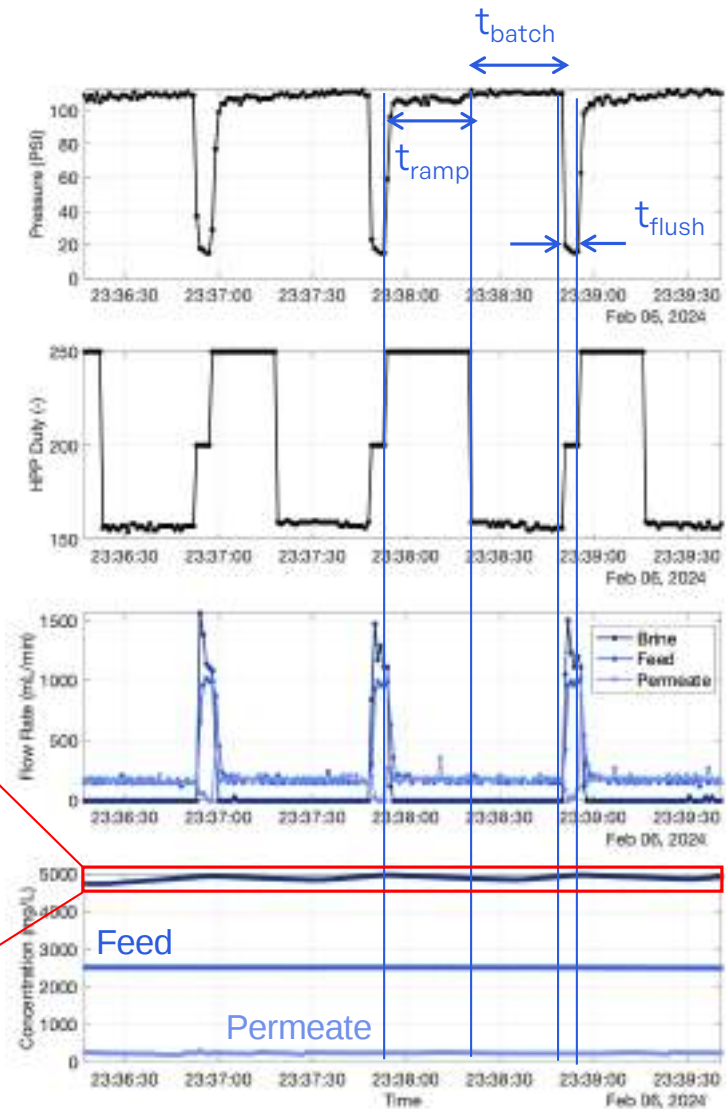
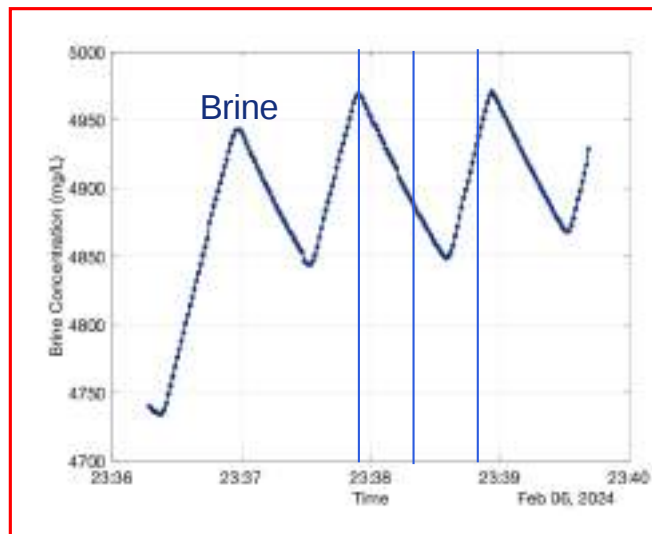
A typical cycle

- Pressure increases (ramp)
- Is regulated (batch)
- And drops (flush)

Results

A typical cycle

- Permeate flow decrease gradually over time
- Conductivity increases over time (ramp & batch)
- Conductivity drops (flush)



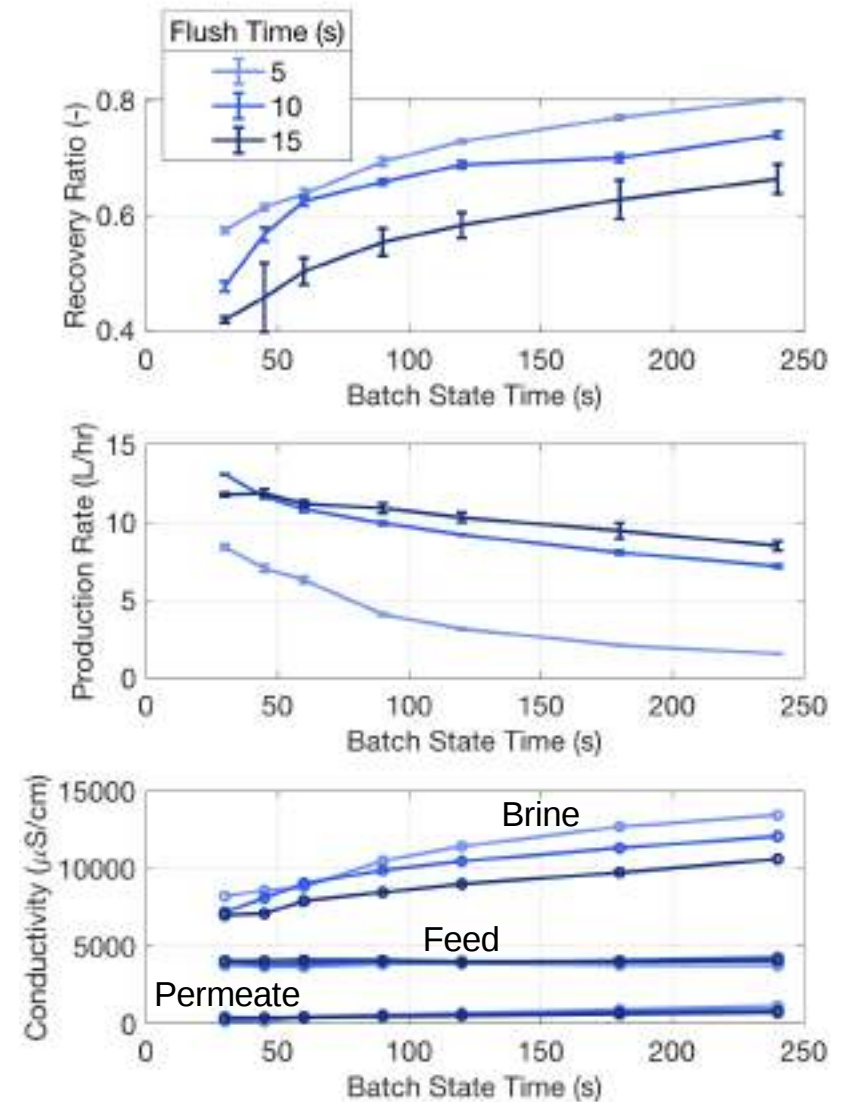
Results

Non-linear tradeoffs

Changing batch time:

- diminishing return on higher recovery
- steep drop in production rate
- higher recirc. loop conductivities

Recall, we want high recovery, high production rate, low recirc. conductivity

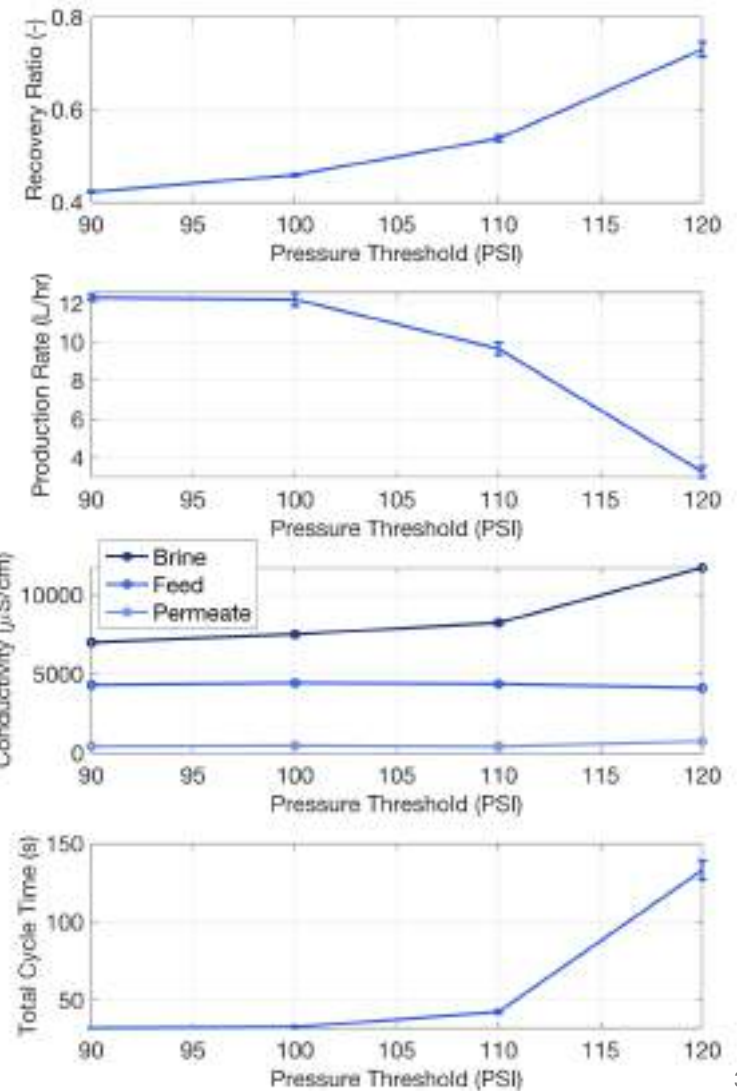


Results

Non-linear tradeoffs

Changing pressures:

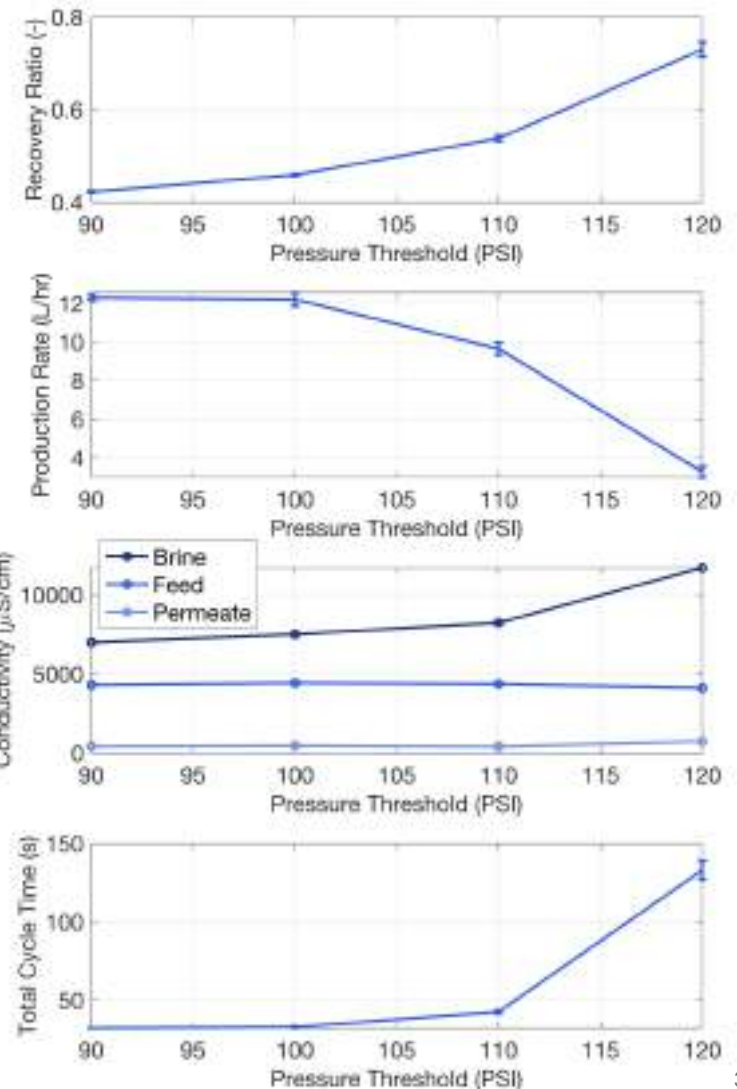
- High recovery
- steep drop in production rate (due to longer batches)
- higher recirc. loop conductivities



Results

Takeaway

- Performance from batch/flush time ratios are relatively coupled, but we want fast batches so lower overall is better.
- There's a sweet spot in batch:flush time (10:1) and operating pressure (~110 PSI)



Conclusions

High-recovery semi-batch architecture

- Relationship between control parameters & performance?
- Withstand scaling & fouling over time?





EUROMED 2024



Desalination for Clean Water and Energy

6–9 May 2024

Four Seasons Hotel, Sharm El Sheikh, Egypt

106

Semi-batch reverse osmosis for home-scale desalination

Jonathan Bessette, S. Shah, M. Ahmedhussain, G. Pertuz, M. Ayoub, & A. Winter

Dept. of Mechanical Engineering, Massachusetts Institute of Technology